AMENDMENTS TO THE CLAIMS:

This listing of claims will replace all prior versions, and listings, of claims in the application:

1. (currently amended) A Process for fluid catalytic cracking of hydrocarbon feedstocks with high levels of basic nitrogen, in multiple riser FCCUs, operating with feedstocks A and B, wherein the process comprises the following steps:

a) place in contact with a zeolite catalyst, in the main riser (7) of the FCCU, ~~hydrocarbon~~ a hydrocarbon feedstock A ~~possessing~~ which possesses a level of basic nitrogen at least 200 ppm lower than feedstock B that is being processed in ~~the secondary~~ a secondary riser (8) of the same FCCU;

b) simultaneously, place in contact with the same zeolite catalyst of a), in said secondary riser (8) of the FCCU, a hydrocarbon feedstock (B) comprised of a mixture made up of between 95 and 40%, in volume, of hydrocarbon ~~stream~~ streams with a ~~percentage~~ content of ~~catalyst damaging~~ catalyst damaging basic nitrogen of between 1000 and 3500 ppm, and between 5 and 60%, by weight, of a cooling fluid capable of increasing the circulation in this secondary riser and of cooling the regenerator, in order to adjust the thermal balance of the FCCU and maintain the circulation of the catalyst in the main riser, at proper levels, so that the catalyst/oil ratio remains in the range of between 4.5 and 8.5;

c) maintain the operation of the FCCU within the conditions of catalytic cracking;

d) recover from tube (10), products of the cracking reaction with an increase in ~~bottom conversion~~ conversion of bottom fractions, a greater proportion of gasoline and LPG, at the same time with a lower proportion of coke and combustible gas.

2. (currently amended) A Process according to claim 1, wherein the FCCU ~~that~~ includes two risers, a main riser and a secondary riser.

3. (currently amended) A Process according to claim 1, wherein ~~an~~ the FCCU that includes three risers, a main and two secondary risers.

4. (currently amended) A Process according to claim 1, wherein said hydrocarbon feedstock A of a) ~~to be made~~ is made up of heavy hydrocarbon streams with a boiling point of between 340°C and 560°C and an °API of between 8 and 28.

5. (currently amended) Process according to claim 4, wherein the heavy hydrocarbon flow streams of feedstock A ~~including~~ comprise vacuum treated heavy gas oil, direct distillation heavy gas oil, atmospheric residue, vacuum residues, deasphalted oil, alone or mixed in any proportion.

6. (currently amended) Process according to claim 5, wherein ~~a heavy~~ one of the heavy hydrocarbon ~~stream~~ streams of A ~~of~~ is a vacuum_treated heavy gas oil with a boiling point of between 380°C and 540°C and an °API of between 15 and 22.

7. (currently amended) Process according to claim 4, wherein the heavy hydrocarbon flow of A ~~including~~ comprises isolated streams and mixtures between streams that have levels of catalyst damaging basic nitrogen of between 200 and 3500 ppm.

8. (currently amended) Process according to claim 1, wherein hydrocarbon feedstock A ~~possessing~~ possesses a level of basic nitrogen of at least 500 ppm lower than feedstock B that is being processed in the secondary riser (8) of the same FCCU.

9. (currently amended) Process according to claim 1, wherein hydrocarbon feedstock A ~~possessing~~ possesses a level of basic nitrogen at least 1000 ppm lower than feed stock B that is being processed in the secondary riser (8) of the same FC0U.

10. (original) Process according to claim 1, wherein hydrocarbon feedstock A

~~possessing~~ possesses a level of basic nitrogen 3500 ppm lower than feedstock B that is being processed in the secondary riser (8) of the same FCCU.

11. (currently amended) Process according to claim 1, wherein the catalyst ~~to be~~ is a conventional zeolite type for FCC processes of heavy feedstocks containing basic nitrogen, with around 30% zeolite dispersed in an inorganic porous carrier.

12. (currently amended) Process according to claim 1, wherein ~~stream~~ feedstock B of hydrocarbons with levels of catalyst damaging basic nitrogen of between 1000 and 3500 ppm of b) ~~to be~~ is a heavy hydrocarbon stream with a boiling point of between 340°C and 560°C and an °API of between 8 and 28.

13. (currently amended) Process according to claim 12, wherein said heavy hydrocarbon stream of feedstock B ~~including~~ includes vacuum treated heavy gas oil, direct distillation heavy gas oil, atmospheric residue, vacuum residues, deasphalted oil, alone or mixed in any proportion.

14. (original) Process according to claim 13, wherein ~~stream B of~~ one of said heavy ~~hydrocarbons~~ hydrocarbon stream of feedstock B to be a deasphalted oil, with an initial boiling point of between 320 and 390°C and an °API of between 12 and 18.

15. (currently amended) Process according to claim 1, wherein the cooling fluid in the secondary riser (8) of b) ~~to be~~ is a light hydrocarbon stream with boiling point between 32 and 350°C and with a density at 20/4°C of between 0.7 and 1.

16. (original) Process according to claim 15, wherein a light hydrocarbon stream is added in proportion of between 5 and 60% by volume of the total stream B.

17. (currently amended) Process according to claim 1, wherein the cooling fluid of the secondary riser (8) of b) ~~to be~~ is an inert stream.

18. (currently amended) Process according to claim 17, wherein ~~an inert stream to be~~ said inert stream is water in proportion of between 5 and 10 % by volume of the total stream B.

19. (currently amended) Process according to claim 1, wherein the hydrocarbon feedstocks A of a) and B of b) ~~to be~~ are introduced into the risers (7) and (8) at temperatures between 100 and 450°C.

20. (currently amended) Process according to claim 19, wherein hydrocarbon feedstocks A of a) and B of b) ~~to be~~ are introduced into the risers (7) and (8) at temperatures of between 240 and 360°C.

21. (currently amended) Process according to claim 1, wherein reaction temperatures in the risers (7) and (8) ~~to be~~ are controlled at between 510 and 570°C.

22. (currently amended) Process according to claim 21, wherein reaction temperatures in the risers (7) and (8) ~~to be~~ are controlled at between 520 and 560°C.

23. (currently amended) Process according to claim 1, wherein the regenerated hot catalyst ~~that it~~ which leaves the regenerator to enter into the risers (7) and (8) to be at temperatures of between 650 and 750°C.

24. (currently amended) Process according to claim 23, wherein the regenerated hot catalyst ~~that it~~ which leaves the regenerator to enter into the risers (7) and (8) to be at temperatures of between 680 and 732°C.

25. (currently amended) Process according to claim 1, wherein the residence time of the catalyst particles, in the risers (7) and (8) ~~to fluctuate~~ fluctuates between 0.3 and 8 seconds.

26. (currently amended) Process according to claim 24, wherein the residence time of the catalyst particles, in the risers (7) and (8) ~~to fluctuate~~ fluctuates between ~~1 and 5~~ one and five seconds.